

(FILE 'USPAT' ENTERED AT 07:36:19 ON 14 SEP 1999)

L1 133291 S ALUMINA OR (ALUMINUM OR ALUMINIUM) (5A) (OXIDE#)
L2 16633 S NICKEL(5A)OXIDE# OR NIO
L3 4542 S L1(P)L2
L4 513 S 423/240R/CCLST
L5 4 S L3 AND L4
L6 236 S 423/240S/CCLST
L7 4 S L3 AND L6

=> s 15 or 17

L8 5 L5 OR L7

=> d 1- cit kwic

1. 5,380,507, Jan. 10, 1995, Method of treating process or flue gases containing halogenous compounds; Matti Hiltunen, et al., **423/240S**; 588/206 [IMAGE AVAILABLE]

US PAT NO: 5,380,507 [IMAGE AVAILABLE]

L8: 1 of 5

US-CL-CURRENT: **423/240S**; 588/206

CLAIMS:

CLMS(4)

4. . . . claim 1 wherein step (b) is practiced to provide as the catalytic material a material selected from zinc oxide, lead **oxide**, iron **oxide**, copper **oxide**, **nickel oxide**, aluminum **oxide**, silicon **oxide**, or mixtures thereof.

2. 4,039,623, Aug. 2, 1977, Catalytic oxidation of C2-C4 halogenated hydrocarbons; Jerome M. Lavanish, et al., **423/240S**, **240R**, 245.3, 481; 588/206, 213 [IMAGE AVAILABLE]

US PAT NO: 4,039,623 [IMAGE AVAILABLE]

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US-CL-CURRENT: **423/240S**, **240R**, 245.3, 481; 588/206, 213

SUMMARY:

BSUM(13)

The **nickel oxide** catalyst can be used in an unsupported form or can be supported on an inert substrate. By "inert" is meant. . . products resulting therefrom. Examples of suitable inert substrates include: asbestos, pumice, activated charcoal, silica gel, colloidal silica, fumed silica, activated **alumina**, and clays. When used in a supported form, the amount of catalyst placed on the support should be sufficient to. . .

DETDESC:

DETD(18)

Approximately 20 cc. of a commercial **nickel (II) oxide** on **alumina** catalyst was dried in a vacuum oven at a temperature of approximately 200.degree. C. and a vacuum of about 27. . . mercury for a period of about 3 hours. The nickel content of this catalyst was about

14 weight percent as **nickel (II) oxide (NiO)** and had a B.E.T. surface area of 140 square meters per gram. X-ray spectroscopic analysis of this commercial catalyst revealed an **alumina** background which masked the **nickel oxide**. 15.2 grams of the dried catalyst was charged to the reactor described in Example II and tested as an incineration. . .

3. 3,943,226, Mar. 9, 1976, Fluids purification; Anthony Miles Robert Difford, 423/230, **240R**, **240S**, 241 [IMAGE AVAILABLE]

US PAT NO: 3,943,226 [IMAGE AVAILABLE]
US-CL-CURRENT: 423/230, **240R**, **240S**, 241

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SUMMARY:

BSUM(13)

In . . . as published by the UK Patent Office) and is preferably nickel or ruthenium. The support of the catalyst is preferably **alumina**. The catalyst is preferably one that has been made by co-precipitation of compounds of nickel and **alumina**. The proportion of nickel in the catalyst, calculated as **nickel oxide NiO** on the **oxide** composition from which the catalyst is made by reduction, is suitably in the range 25- 90, especially 40- 75%, by. . .

DETDESC:

DETD(12)

An . . . extruded cylinders 0.125 inch in diameter and 0.25 to 0.5 inch in length of a hydrosulphurisation catalyst consisting of sulphided **nickel oxide** and molybdenum **oxide** on **alumina** and then, over and in contact with that catalyst, 100 ml (i.e. 86 g) of sodium beta aluminate/**alumina** granules from a works-scale repeat of the preparation described in Example 1(a). The reactor was fed with a mixture at. . .

4. 3,935,295, Jan. 27, 1976, Process for removing chlorine-containing compounds from hydrocarbon streams; Richard W. La Hue, et al., **423/240R**; 208/226, 262.1; 423/230 [IMAGE AVAILABLE]

US PAT NO: 3,935,295 [IMAGE AVAILABLE]
US-CL-CURRENT: **423/240R**; 208/226, 262.1; 423/230

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DETDESC:

DETD(9)

The . . . entered the reactor 3 through line 1. The reactor contained 15 cc. of CCI's C20-7 catalyst. This catalyst consists of **nickel** and molybdenum **oxides** on activated **alumina**. The hydrogen treated feed was passed through line 5 and inlet samples were drawn off daily through sample point 6.. . .

DETDESC:

DETD(16)

Now . . . 16 mesh particles of a commercial hydrotreating catalyst sold by Catalysts & Chemicals, Inc. This catalyst, known as C20-7, contains **nickel oxide** in a percentage by weight of 3.8 and molybdenum oxide in a concentration by weight of 14.1 percent on an **alumina** support. It has a surface area of 150 m.sup.2 /gm. This material formed a catalyst bed 4 in the catalyst. . .

5. 3,892,818, Jul. 1, 1975, Catalytic conversion of hydrocarbon

chlorides to hydrogen chloride and hydrocarbons; Gerhard Scharfe, et al.,
423/481, **240R**, **240S**; 502/170, 184, 185, 325; 585/357, 359, 434,
469, 612, 641, 733, 935; 588/209, 213 [IMAGE AVAILABLE]

US PAT NO: 3,892,818 [IMAGE AVAILABLE]

L8: 5 of 5

US-CL-CURRENT: 423/481, **240R**, **240S**; 502/170, 184, 185, 325;
585/357, 359, 434, 469, 612, 641, 733, 935; 588/209, 213

DETDESC:

DETD(23)

d. 0.9 % by wt. of rhodium and 0.1 % **nickel** on **aluminum**
oxide;